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BIOETHANOL TO HYDROGEN MEMBRANE SURFACE CHARACTERISTICS CHANGE STUDY

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ИЗМЕНЕНИЕ ПОВЕРХНОСТНЫХ ХАРАКТЕРИСТИК КАТАЛИТИЧЕСКИХ МЕМБРАН ПРЕВРАЩЕНИЯ БИОЭТАНОЛА В ВОДОРОД

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Abstract. The problem of the gradual transformation of the modern economy towards greater production and consumption of 'green' energy requires a significant revision of existing technologies. One of the possible ways to develop green energy is the use of hydrogen as the most environmentally friendly fuel. Hydrogen can be obtained both by electrolysis, using solar energy, and using biorenewable raw materials, which can be used as ethanol, biogas, peat, agricultural waste. At the same time, for regions with a low level of illumination, the production of hydrogen by electrolysis of water using electricity generated by solar panels is inaccessible, and therefore the processing of biorenewable raw materials can take a leading position. Bioethanol is a large-capacity product with a proven production technology that widely uses waste from agriculture and wood processing. Ethanol can be used as a feedstock for hydrogen generation by means of catalytic pyrolysis or catalytic steam reforming. Membrane-catalytic steam reforming of ethanol with the production of hydrogen makes it possible to obtain hydrogen without the use of an additional purification step, however, the efficiency and stability of the membrane becomes the determining parameter that ensures the efficiency of the entire process. The degradation of inorganic membranes during catalytic steam reforming is closely related to the change in porosity as a result of hydrolysis of the membrane surface. In this connection, the study of the physicochemical properties of membranes during operation can make a significant contribution to the development of stable catalytic membranes for hydrogen production. The article presents the results of studying the physicochemical properties of an inorganic membrane for ethanol steam reforming by the method of low-temperature nitrogen adsorption. The Langmuir, Brunauer-Emmett-Taylor, t-plot and Barrett-Joyner-Halenda models were used to estimate the surface change. An increase in the surface area of mesopores during the operation of the membrane was determined.

Аннотация. Проблема постепенной трансформации современной экономики в сторону большего производства и потребления «зеленой» энергии требует существенного пересмотра существующих технологий. Одним из возможных путей развития зеленой энергетики является использование водорода как наиболее экологически чистого топлива. Водород может быть получен как методом электролиза, с использованием энергии солнца, так и с использованием биовозобновляемого сырья, в качестве которого возможно использование этанола, биогаза, торфа, отходов сельского хозяйства. При этом для регионов с низким уровнем освещенности получение водорода электролизом воды с использованием электроэнергии, вырабатываемой солнечными батареями, является недоступным, в связи с чем переработка биовозобновляемого сырья может занять лидирующие позиции. Биоэтанол является крупнотоннажным продуктом с отработанной технологией производства, широко использующей отходы сельского хозяйства и переработки древесины. Этанол может быть использован в качестве сырья для выработки водорода по средствам каталитического пиролиза или каталитической паровой конверсии. Мембранно-каталитическая паровая конверсия этанола с получением водорода позволяет получить водород без использования дополнительной стадии очистки, однако, эффективность и стабильность работы мембраны становится определяющим параметром, обеспечивающим эффективность работы всего процесса. Дегградация неорганических мембран в процессе каталитической паровой конверсии тесным образом связана с изменением пористости в результате гидролиза поверхности мембраны. В связи с чем изучения физико-химических свойств мембран в процессе работы может дать существенный вклад в разработку стабильных каталитических мембран получения водорода. В статье приводятся результаты изучения физико-химических свойств неорганической мембраны паровой конверсии этанола методом низкотемпературной адсорбции азота. Для оценки изменения поверхности были использованы модели Ленгмюра, Брунауэра-Эммета-Тейлора, t-график и модель Баррета-Джойнера-Халенды. Определено увеличение площади поверхности мезопор в процессе функционирования мембраны.

Keywords: membranes, adsorption, bioenergy.

Ключевые слова: мембраны, адсорбция, биоэнергия.

Introduction

Green and sustainable economy determine essential demand for green energy production [1, 2]. One possible way to solve this problem is to develop method for hydrogen production from renewable resources [3, 4]. Green hydrogen can be produced using water electrolysis and bio renewable resources catalytic pyrolysis, gasification and transformation [5]. Bioethanol can be considered as bio renewable resource easily produce from agriculture and wood processing wastes and applicable for hydrogen production [6, 7]. Bioethanol can be converted into hydrogen using ethanol water gas shift reaction. Efficiency of the process is determined catalysts activity and selectivity [8]. Typically, Pt, Pd, Ni, Fe, Cu, Zn, Al containing catalysts are used to provide this process [9]. Catalytic process of bioethanol to hydrogen transformation can be combined with membrane proses of hydrogen separation [10]. The main problem of such systems is catalyst deactivation due to surface carbonization and active metals degradation [11]. Therefor insight in surface change during catalytic membrane operation is essential for understanding ways to decrease membranes deactivation.

Nitrogen physisorption can be considered as effective method for obtaining membranes surface characteristics and determination of surface change during membrane work. Typically,

nitrogen physisorption measurements are provided using static volumetric method, were nitrogen adsorption determined by mass balance equations and pressure drop in sample cell. For evaluation of obtained data several models can be used including Langmuir, BET, BJH [12] and t-plot methods can be used. Langmuir model includes adsorption of one molecular layer on solid surface (1).

$$\frac{P}{V_a} = \frac{1}{V_m b} + \frac{P}{V_m} \quad (1)$$

Where p — system pressure, Pa; V_a — volume of adsorbed gas; V_m — volume of adsorbed gas forms monomolecular layer; b — correlation coefficient.

Most frequently used Brunauer, Emmett, and Teller model includes possibility of gas multilayer condensation (2).

$$\frac{P}{V_a(P_0 - P)} = \frac{1}{V_m C} + \frac{C - 1}{V_m C} \left(\frac{P}{P_0} \right) \quad (2)$$

Where P_0 — saturation pressure of gas; C — gas adsorption constant; Barrett-Joyner-Halenda (BJH) method is based on Kelvin equation (3).

$$\frac{RT}{v} \ln \left(\frac{p}{p_0} \right) = \sigma C \quad (3)$$

Where v — molar volume; σ — liquid surface tension; C — is mean curvature defined on formula 4.

$$C = \frac{1}{r_1} + \frac{1}{r_2} \quad (4)$$

Where r — interfacial curvature;

The equation 4 can be converted into equation 5.

$$\ln \frac{P}{P_0} = - \frac{2\gamma v \cos\theta}{r_k RT} \quad (5)$$

Where γ — interfacial tension, θ — contact angle of condensed liquid with wall.

t-plot model uses equation (6) to evaluate micropores volume, external surface area and micropore surface area.

$$t = \sqrt{\frac{13.99}{\log_{10} \left(\frac{p_0}{p} \right) + 0.034}} \quad (6)$$

where t — film thickness;

Application of discussed models for surface characterization gives possibility for evaluation of membranes surface degradation during its work.

Materials and Methods

Specific surface area and porosity were determined using the following instruments: Becman coulter SA3100 surface area and pore size distribution analyzer (Coulter corporation, Miami, Florida), sample preparation device: Becman coulter SA-prep (Coulter corporation, Miami, Florida). For analysis, the sample is placed in a pre-weighed quartz cuvette, which is installed in the SA-PREP™ sample preparation instrument. Sample preparation parameters: temperature — 120°C; gas — nitrogen; preparation time — 60 min. After completion of sample preparation, the cuvette is

cooled and weighed, and then transferred to the analytical port of the BECMAN COULTER SA 3100™ instrument. Gas was sequentially supplied to the analytical cell and the equilibrium pressure in the system was determined.

Results and Discussions

Initial membrane characterized by Langmuir surface area 1.3 m²/g, BET surface area 2.9 m²/g, t-plot surface area 25.3 m²/g. BJH-pore volume distribution (Figure 1) shows that most part of mesopores have diameter less than 6 nm.

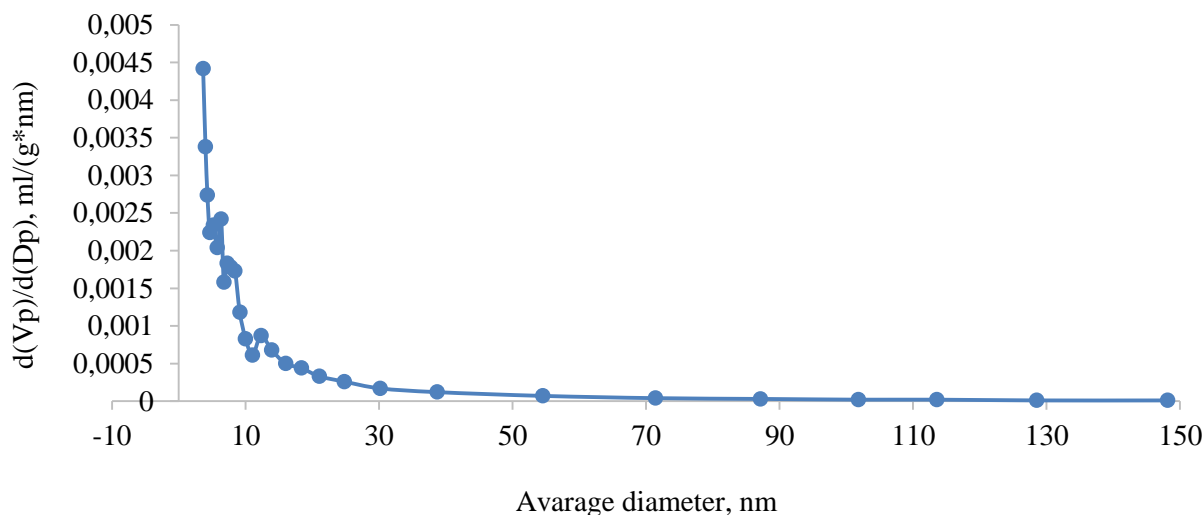


Figure 1. Pore volume distribution for initial inorganic membrane

Membrane operation for 50 h on stream results in increase of Langmuir surface area 4.7 m²/g, BET surface area up to 12.3 m²/g, t-plot surface area 78.4 m²/g. BJH-pore volume distribution (Figure 2) shows shift of average pore diameter to 20 nm.

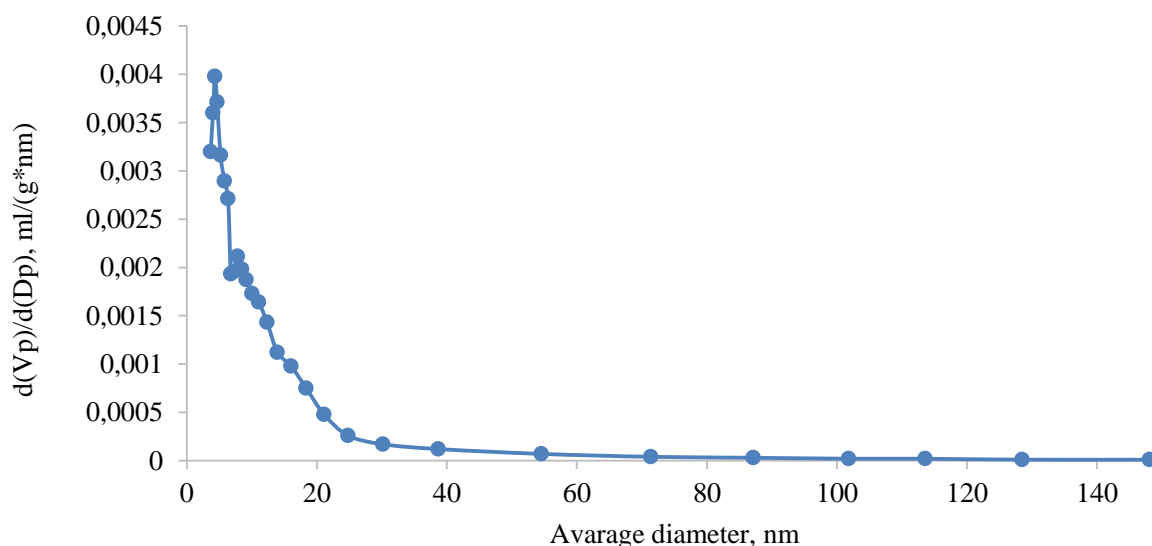


Figure 2. Pore volume distribution for membrane from ethanol to hydrogen reaction operation for 50 h on stream

Membrane operation for 100 h on stream results in increase of Langmuir surface area 7.4 m²/g, BET surface area up to 24.9 m²/g, t-plot surface area 53.9 m²/g. BJH-pore volume distribution (Figure 3) shows small shift of average pore diameter to region less than 15 nm.

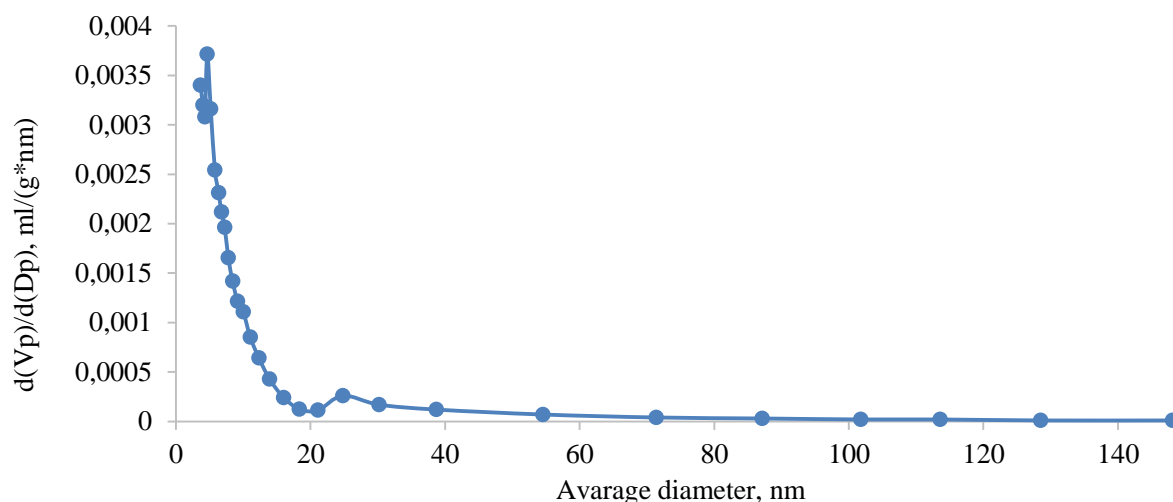


Figure 3. Pore volume distribution for membrane from ethanol to hydrogen reaction operation for 100 h on stream

Membrane surface degradation during methanol to hydrogen reaction process shows partial increase of membrane mesoporosity and microporosity that can be explained by partial hydrolysis of membrane surface with water steam forming during ethanol to hydrogen transformation process.

Conclusions

Membrane surface degradation is a complex problem for inorganic catalytic membranes. Ethanol to hydrogen catalytic transformation process provided on inorganic membranes strongly suffers from membrane degradation because of high exothermic effect and high amount of water forming during the process. After 50 hours on stream Langmuir surface area increase from 1.3 m²/g to 4.7 m²/g, BET surface area increase form 2.9 m²/g to 12.3 m²/g and t-plot surface area increase from 25.3 m²/g to 78.4m²/g. After 100 hours on stream Langmuir surface area increase to 7.4 m²/g, BET surface area increase to 24.9 m²/g and t-plot surface area decrease to 53.9m²/g.

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